

CHAPTER 6. INVISCID COMPRESSIBLE FLOW

1. Bernoulli equation for gases. Saint-Venant equation
2. Different behaviour of compressible fluid and incompressible fluid in isentropic flow
3. Concepts: generator state, stagnation state, critical state, limit velocity
4. Hugoniot's theorems. Application to the design of nozzles and diffusers

1. Bernoulli equation for gases: Saint - Venant

1. Isentropic flow. Saint-Venant equation
2. Speed of sound
3. Saint-Venant equation, dimensionless form

1.1. Isentropic flow. Saint-Venant equation

- ✓ Hypotheses
- ✓ Differential energy equation of the steady-state flow of perfect gases

- Bernoulli:
$$\int_1^2 \frac{dp}{\rho} + \frac{1}{2}(U_2^2 - U_1^2) + g(z_2 - z_1) = 0$$
 "Bernoulli equation in a compressible fluid" (steady-state regime) valid for a streamline.

$$\frac{U^2}{2} + gz + \int \frac{dp}{\rho} = \text{Cte} \quad \Rightarrow \quad \rho U dU + dp = 0$$

- ✓ Saint - Venant equation:


$$\left. \begin{array}{l} \rho U dU + dp = 0 \\ p = C \rho^k \end{array} \right\} \Rightarrow \frac{U^2}{2g} + \frac{k}{k-1} \frac{p}{\gamma} = \text{Cte} \quad \text{Saint-Venant equation (1st form)}$$

$$\frac{U^2}{2g} + \frac{k}{k-1} R' T = \text{Cte} \quad \text{Saint-Venant equation (2nd form)}$$

$$c_p' (\text{m/K}) = \frac{c_p (\text{J/k} \cdot \text{mol})}{(A \cdot 10^{-3}) (\text{kg/mol}) \cdot g (\text{m/s}^2)} \quad \frac{U^2}{2g} + c_p' T = \text{Cte} \quad \text{Saint-Venant equation (3rd form)}$$

1.1. Isentropic flow. Saint-Venant equation

- ✓ Saint - Venant equation, between 2 points

$$\boxed{\frac{U^2}{2g} + \frac{k}{k-1} \frac{p}{\gamma} = \text{Cte}}$$
$$\boxed{p = C\rho^k}$$

$$\boxed{\frac{U_1^2 - U_2^2}{2g} = \frac{k}{k-1} \frac{p_1}{\gamma_1} \left[\left(\frac{p_2}{p_1} \right)^{\frac{k-1}{k}} - 1 \right]}$$

- Alternative expressions:

$$\boxed{\frac{U_1^2 - U_2^2}{2g} = \frac{k}{k-1} \frac{p_1}{\gamma_1} \left[\left(\frac{\gamma_2}{\gamma_1} \right)^{k-1} - 1 \right]}$$

$$\boxed{\frac{U_1^2 - U_2^2}{2g} = \frac{k}{k-1} R'(T_2 - T_1)}$$

$$\boxed{\frac{U_1^2 - U_2^2}{2g} = c_p'(T_2 - T_1)}$$

1.2. Speed of sound

✓ Definition

✓ Newton's formula for the speed of sound:

$$c^2 = \frac{dp}{d\rho} = \frac{E_v}{\rho}$$

✓ Example

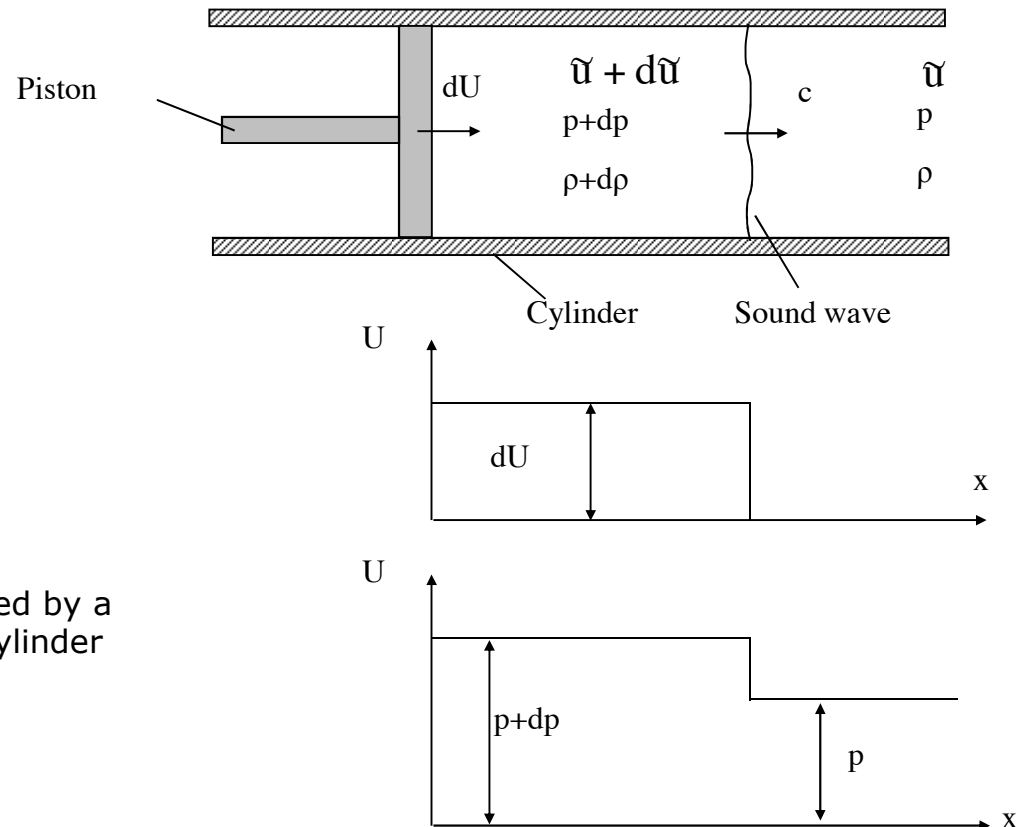


Figure 6.1 Disturbance generated by a piston on a static fluid inside a cylinder

1.2. Speed of sound

✓ Mach number:

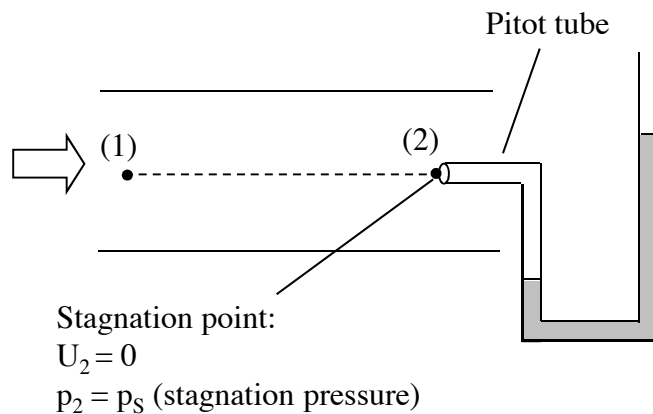
$$M = \frac{U}{c}$$

- Flow regime classification:
 - Subsonic regime: $M < 1$, $U < c$
 - Sonic regime or critical regime: $M = 1$, $U = c$
 - Supersonic regime: $M > 1$, $U > c$

1.3. Saint-Venant equation, dimensionless form

✓ Saint – Venant equation, as a function of Mach No.

$$\frac{U_1^2 - U_2^2}{2g} = \frac{k}{k-1} \frac{p_1}{\gamma_1} \left[\left(\frac{p_2}{p_1} \right)^{\frac{k-1}{k}} - 1 \right] \quad \Rightarrow \quad \frac{1}{2} \frac{U^2}{c^2} = \frac{1}{k-1} \left[\left(\frac{p_S}{p} \right)^{\frac{k-1}{k}} - 1 \right]$$



$$\frac{p_S}{p} = \left[1 + \frac{k-1}{2} M^2 \right]^{\frac{k}{k-1}}$$

“Saint-Venant equation as a function of the Mach No.”

Figure 6.3 Pitot tube in a fluid flow

1.3. Saint-Venant equation, dimensionless form

$$\frac{p_s}{p} = \left[1 + \frac{k-1}{2} M^2 \right]^{\frac{k}{k-1}}$$

NEWTON BINOMIAL:

$$(a + x)^\alpha = a^\alpha \sum_{n=0}^{\infty} \binom{\alpha}{n} \left(\frac{x}{a}\right)^n = a^\alpha \sum_{n=0}^{\infty} \frac{\alpha(\alpha-1)\dots(\alpha-n+1)}{n!} \left(\frac{x}{a}\right)^n$$

$$\binom{\alpha}{n} = \frac{\alpha!}{(\alpha-n)!n!}$$

$$\alpha = \frac{k}{k-1}$$

$$a = 1$$

$$x = \frac{k-1}{2} M^2$$



$$\frac{p_s}{p} = 1 + \frac{k}{2} M^2 + \frac{k}{8} M^4 + \frac{k(2-k)}{48} M^6 + \dots$$



$$\frac{p_s - p}{\frac{1}{2} \rho U^2} = 1 + \frac{M^2}{4} + \frac{2-k}{24} M^4 + \dots$$

“Saint – Venant equation, dimensionless form”

2. Different behaviour of compressible fluid and incompressible fluid in isentropic flow

$$\frac{p_s - p}{\frac{1}{2}\rho U^2} = 1 + \frac{M^2}{4} + \frac{2-k}{24}M^4 + \dots$$

Saint - Venant equation, in dimensionless form

$$\frac{p_s - p}{\frac{1}{2}\rho U^2} = 1$$

Bernoulli equation, in dimensionless form

M	$\frac{p_s - p}{\frac{1}{2}\rho U^2}$	
0	1	Incompressible case
0,1	1,003	Equivalent to incompressible
0,2	1,010	
0,3	1,023	Compressible case
0,4	1,041	

Conclusion: a gas can be considered as incompressible fluid for a Mach number of $M < 0.2$ by admitting an error smaller than 1% in the dimensionless form of the Saint-Venant equation

3. Concepts: generator state, stagnation state, critical state, limit velocity

- ✓ Generator state (0)
- ✓ Stagnation state (S)

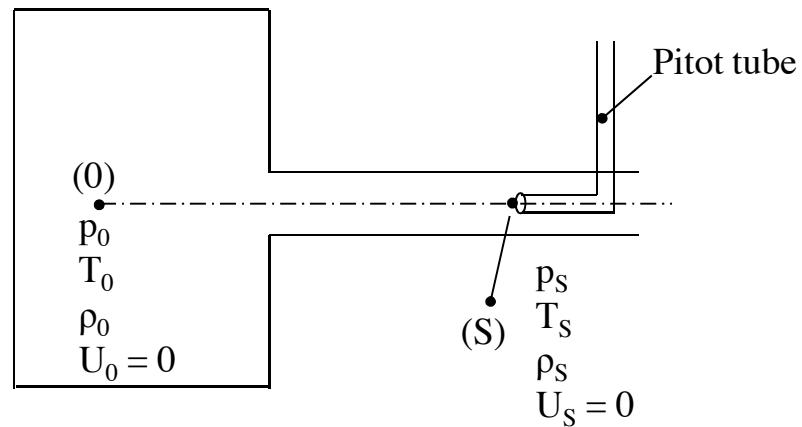


Figure 6.4 Generator state and stagnation point

3. Concepts: generator state, stagnation state, critical state, limit velocity

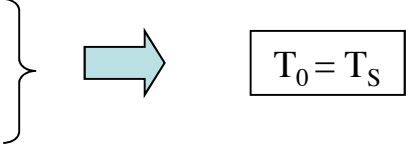
- ✓ Perfect fluid, isentropic flow

Stagnation state (S) = Generator state (0)

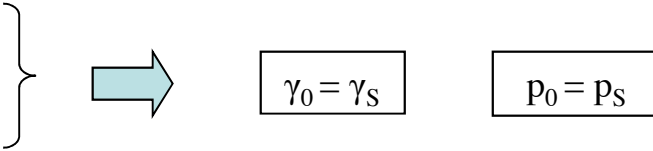
$$\left\{ \begin{array}{l} p_0 = p_s \\ \gamma_0 = \gamma_s \\ T_0 = T_s \end{array} \right\}$$

- ✓ Demonstration

- Saint - Venant (0)-(S)
- Ideal gas


$$T_0 = T_s$$

- Isentropic flow
- Ideal gas


$$\gamma_0 = \gamma_s \quad p_0 = p_s$$

3. Concepts: generator state, stagnation state, critical state, limit velocity

✓ Generator state, Mach functions

$$\frac{p_0}{p} = \left[1 + \frac{k-1}{2} M^2 \right]^{\frac{k}{k-1}}$$

$$\frac{\gamma_0}{\gamma} = \left[1 + \frac{k-1}{2} M^2 \right]^{\frac{1}{k-1}}$$

$$\frac{T_0}{T} = \left[1 + \frac{k-1}{2} M^2 \right]$$

$$\left[1 + \frac{k-1}{2} M^2 \right] = \frac{T_0}{T} = \left(\frac{p_0}{p} \right)^{\frac{k-1}{k}} = \left(\frac{\gamma_0}{\gamma} \right)^{k-1}$$

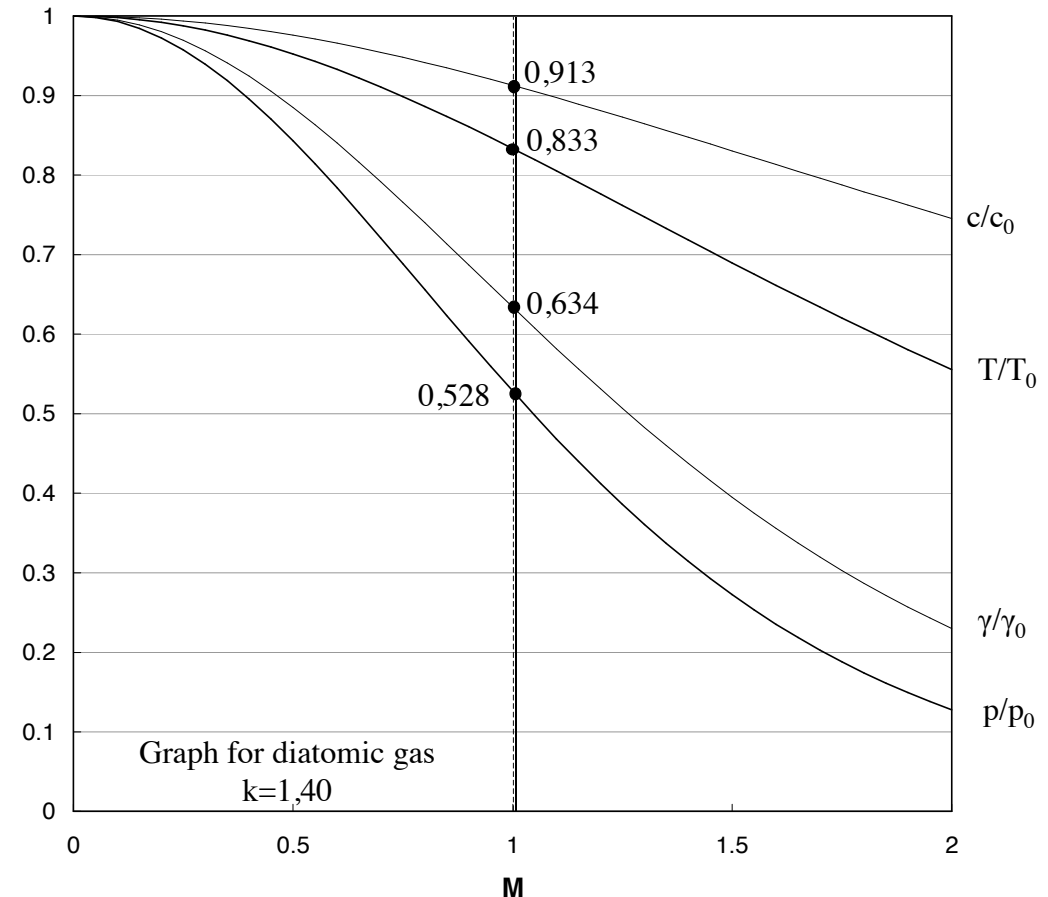


Figure 6.5 Characteristic variables of the flow with respect to the generator state, as a function of Mach no.

3. Concepts: generator state, stagnation state, critical state, limit velocity

✓ Critical state

$$\frac{p_0}{p} = \left[1 + \frac{k-1}{2} M^2 \right]^{\frac{k}{k-1}}$$

$$\frac{\gamma_0}{\gamma} = \left[1 + \frac{k-1}{2} M^2 \right]^{\frac{1}{k-1}}$$

$$\frac{T_0}{T} = \left[1 + \frac{k-1}{2} M^2 \right]$$



$$\frac{p_0}{p_c} = \left[\frac{k+1}{2} \right]^{\frac{k}{k-1}}$$

$$\frac{\gamma_0}{\gamma_c} = \left[\frac{k+1}{2} \right]^{\frac{1}{k-1}}$$

$$\frac{T_0}{T_c} = \left[\frac{k+1}{2} \right]$$



**Diatomic gas
(k=1,4)**

$$\frac{T_c}{T_0} = 0,833$$

$$\frac{\gamma_c}{\gamma_0} = 0,634$$

$$\frac{p_c}{p_0} = 0,528$$

3. Concepts: generator state, stagnation state, critical state, limit velocity

✓ Limit velocity

- Saint – Venant (0)-(lim)

$$U_{\text{lim}} = c_0 \sqrt{\frac{2}{k-1}}$$

3. Experimental characterization of a gas flow

✓ Variables

- 1- Mach no.: "M"
- 2- Temperature: "T"
- 3- Speed of sound: "c"
- 4- Fluid velocity: "U"
- 5- Fluid density: "ρ"
- 6- Mass flow rate: "q_m"

✓ Measurements

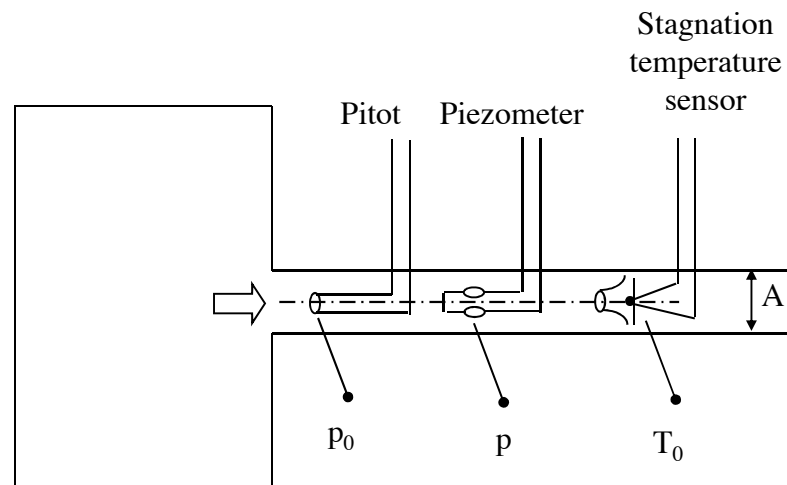


Figure 6.6 Characterization of a gas flow

3. Experimental characterization of a gas flow

- ✓ Scheme of calculation

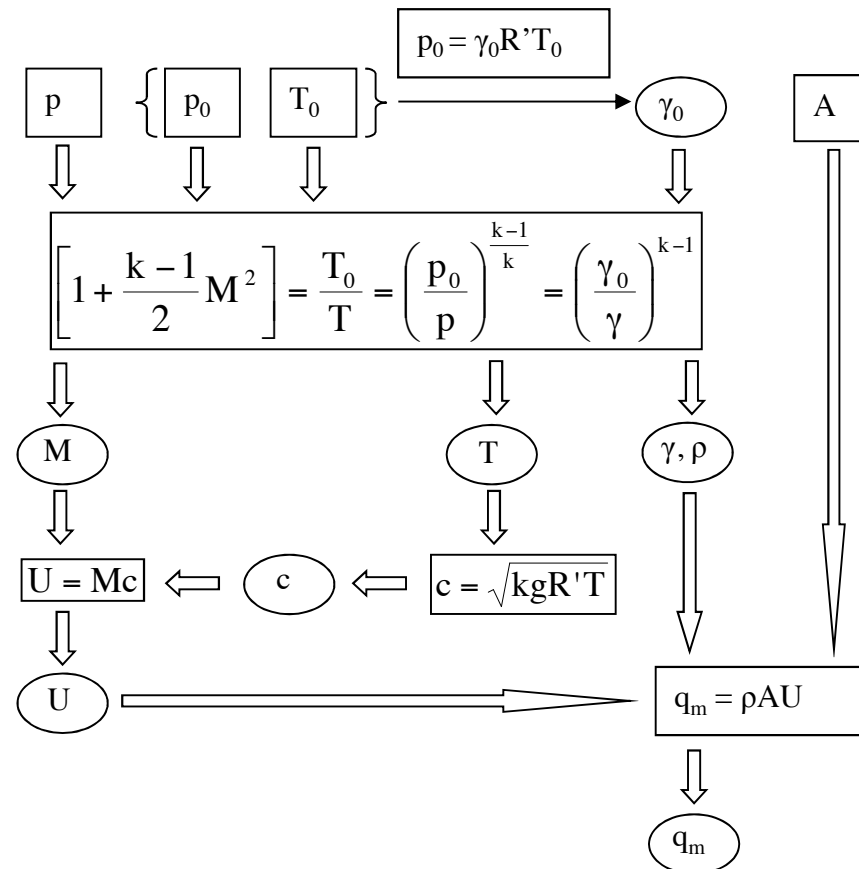


Figure 6.7 Scheme of calculation in a standard problem with a gas flow

4. Hugoniot's theorems

- ✓ Formulation of the theorems (4)
- ✓ Hugoniot's equations (2)

$$\frac{dA}{A} = \frac{dU}{U} (M^2 - 1)$$

$$\frac{dU}{U} = -\frac{1}{kM^2} \frac{dp}{p}$$

- ✓ Proof of the equations

- Continuity equation

$$q_m = \text{Cte} = \rho AU$$



$$0 = \frac{d\rho}{\rho} + \frac{dA}{A} + \frac{dU}{U}$$

- Energy equation

$$\rho U dU + dp = 0$$

- Newton's formula for the speed of sound

$$c^2 = \frac{dp}{d\rho}$$



$$\frac{dA}{A} = \frac{dU}{U} (M^2 - 1)$$

EQUATION 1

4. Hugoniot's theorems

✓ Proof of the equations

- Energy equation

$$\rho U dU + dp = 0$$

- Newton's formula for the speed of sound

$$c^2 = \frac{kp}{\rho}$$



$$\frac{dU}{U} = -\frac{1}{kM^2} \frac{dp}{p}$$

EQUATION 2

4. Hugoniot's theorems

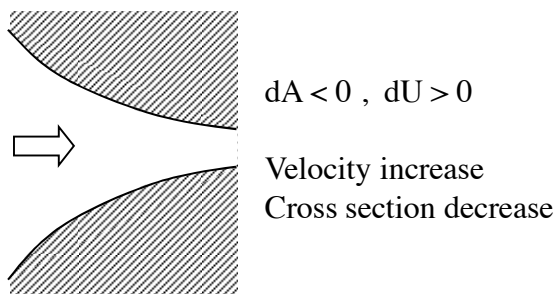
- ✓ Physical interpretation of the equations

$$\frac{dA}{A} = \frac{dU}{U} (M^2 - 1)$$

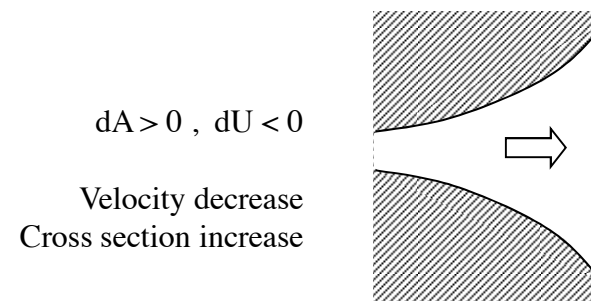
EQUATION 1

- Theorem 1: Subsonic regime: $M < 1$

(M^2-1)	dU	dA	
(-)	(+)	(-)	CASE A
(-)	(-)	(+)	CASE B



CASE A: Convergent nozzle



CASO B: Divergent diffuser

4. Hugoniot's theorems

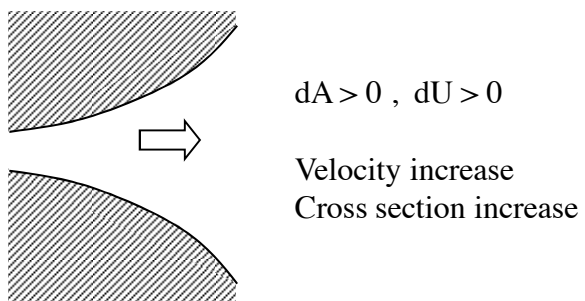
- ✓ Physical interpretation of the equations

$$\frac{dA}{A} = \frac{dU}{U} (M^2 - 1)$$

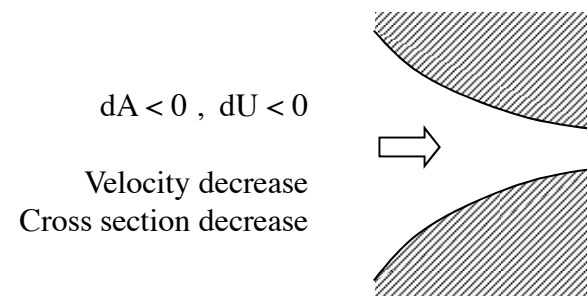
EQUATION 1

- Theorem 2: Supersonic regime: $M > 1$

(M^2-1)	dU	dA	
(+)	(+)	(+)	CASE C
(+)	(-)	(-)	CASE D



CASE C: Divergent nozzle



CASE D: Convergent diffuser

4. Hugoniot's theorems

- ✓ Interpretation of the equations

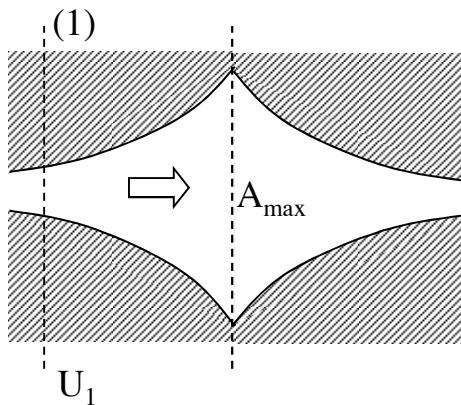
$$\frac{dA}{A} = \frac{dU}{U} (M^2 - 1)$$

EQUATION 1

- Theorem 3: Sonic regime: $M = 1$

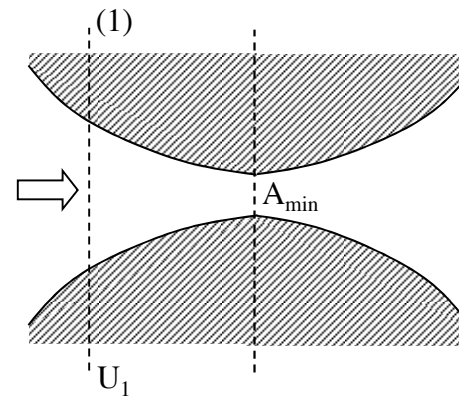
$$\frac{dA}{A} = 0$$

Case: A_{\max}



IMPOSSIBLE

Case: A_{\min}



POSSIBLE

4. Hugoniot's theorems

- ✓ Physical interpretation of the equations

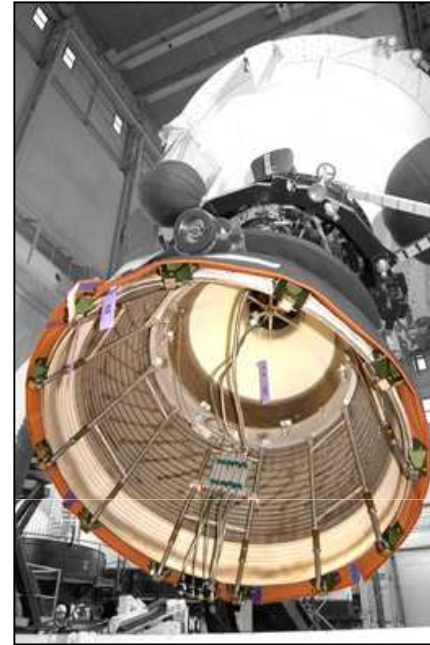
$$\frac{dU}{U} = -\frac{1}{kM^2} \frac{dp}{p}$$

EQUATION 2

- Theorem 4: if $dU > 0$ then $dp < 0$ and if $dU < 0$ then $dp > 0$

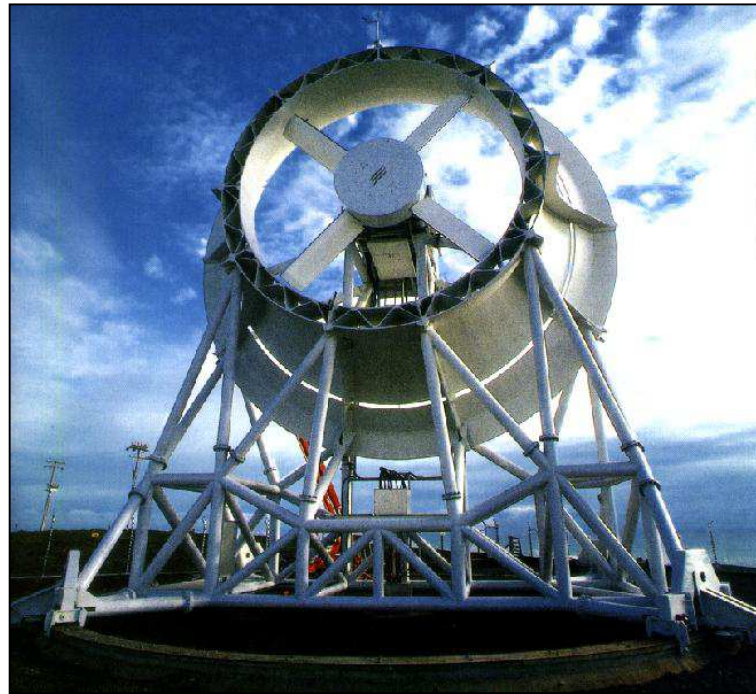
4. Design of nozzles and diffusers

- ✓ Concept: Nozzle

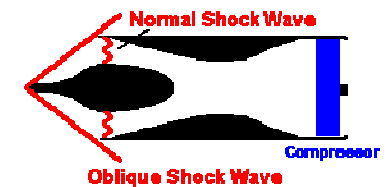
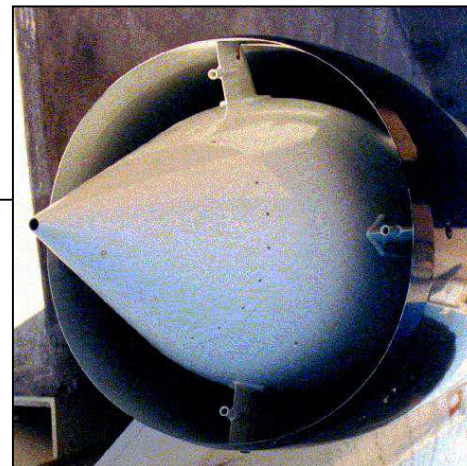
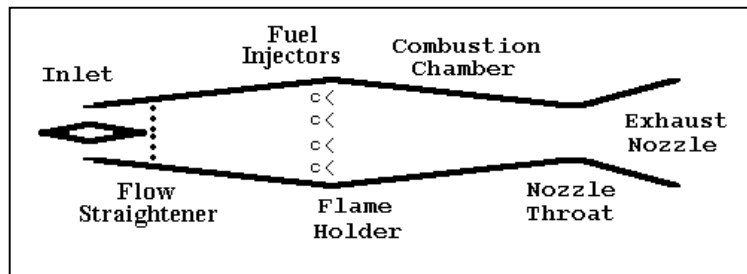


4. Design of nozzles and diffusers

✓ Concept: Diffuser



Center Body Diffuser



The center body can be mounted on tracks. It must be moved further out as the aircraft flies faster.

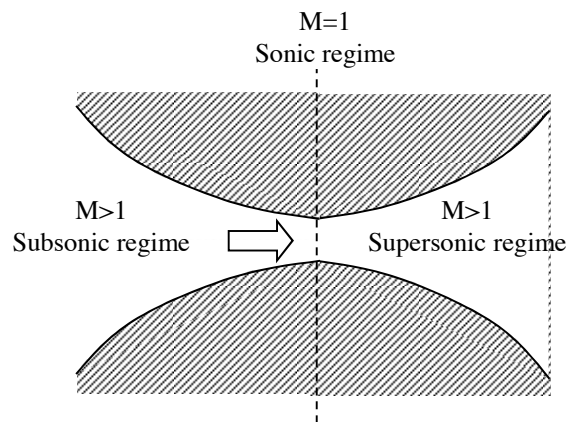
4. Design of nozzles and diffusers

✓ Nozzle

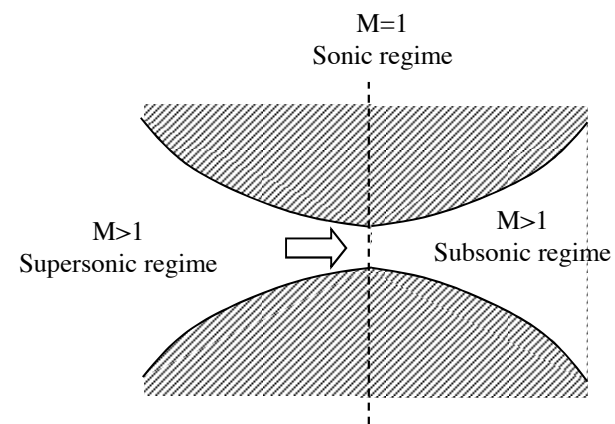
		(M^2-1)	dU	dA	dp	dT	$d\rho$	
Subsonic regime	$M < 1$	(-)	(+)	(-)	(-)	(-)	(-)	CASE A (convergent)
Supersonic regime	$M > 1$	(+)	(+)	(+)	(-)	(-)	(-)	CASE C (divergent)

✓ Diffuser

		(M^2-1)	dU	dA	dp	dT	$d\rho$	
Subsonic regime	$M < 1$	(-)	(-)	(+)	(+)	(+)	(+)	CASE B (divergent)
Supersonic regime	$M > 1$	(+)	(-)	(-)	(+)	(+)	(+)	CASE D (convergent)



Convergent-divergent nozzle (Laval)



Convergent-divergent diffuser